

# Solid Oxide Fuel Cell Research at the University of Waterloo

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#### **Supervised By**

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## Introduction



- UW and CANMET have been involved in research on clean energy from fossil fuels for many years/decades
- Focus in recent years has been on CO<sub>2</sub> mitigation technologies
  from fossil-fuel based power plants
  - Higher efficiency power plant
  - $\succ$  CO<sub>2</sub> capture and storage (energy intensive, costly)
- SOFC appears very promising in terms of efficiency and reduced cost of capturing CO<sub>2</sub>

#### **SOFC Research at Waterloo**



- SOFC Research at Waterloo started in 2001
  - 2 published research papers and 1 about to be submitted
- Main activity: computer simulation
  - Process simulation (Aspen Plus)
  - Fundamental single cell modeling (Matlab, Femlab)
- Current focus:
  - SOFC power generation from coal/natural gas
  - $\succ$  Effect of mixtures of CO/H<sub>2</sub> on cell performance
  - > CO<sub>2</sub> capture from SOFC systems
- Collaboration with CANMET Energy Technology Centre

### **SOFC Research at Waterloo - Personnel**



- Supervisors:
  - Eric Croiset, assistant professor
  - Peter Douglas, professor
  - Michael Fowler, lecturer
  - Evgueniy Entchev, research scientist, CANMET
- Graduate students:
  - Rapeepong Suwanwarangkul, Ph.D. candidate
  - Wei Zhang, M.A.Sc. candidate
  - Leslie Backham, M.A.Sc. candidate

## **Overall Research Objective**



Investigate/develop SOFC-based power generation processes that can simultaneously:

> achieve high electricity generation efficiencies

> generate pure CO<sub>2</sub> with minimum energy/cost penalty

## Key Issues to be Investigated



- Key operating variables:
  - fuel composition (Especially H<sub>2</sub> and CO mixtures)
  - utilization factor
  - temperature
  - pressure
  - operating cell voltage or current density
- Cycle options for CO<sub>2</sub> capture and concentration
  oxygen enrichment, chemical absorption
- Efficiency and cost

#### **Overall Research Methodology**



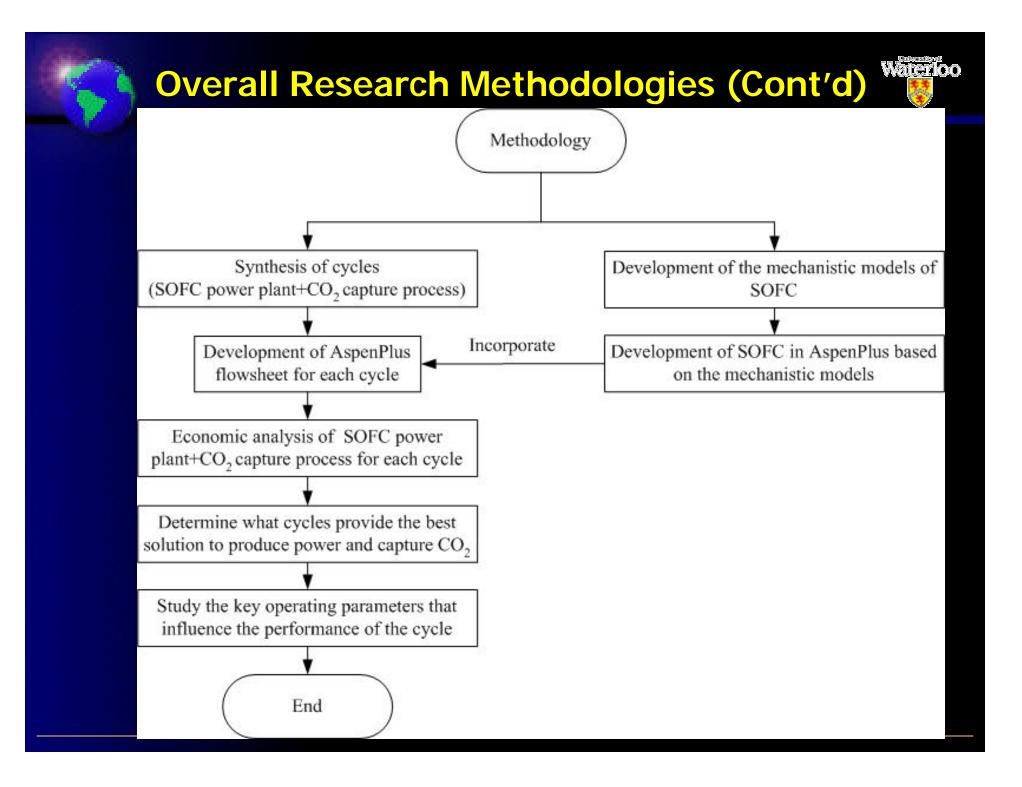
#### Synthesis:

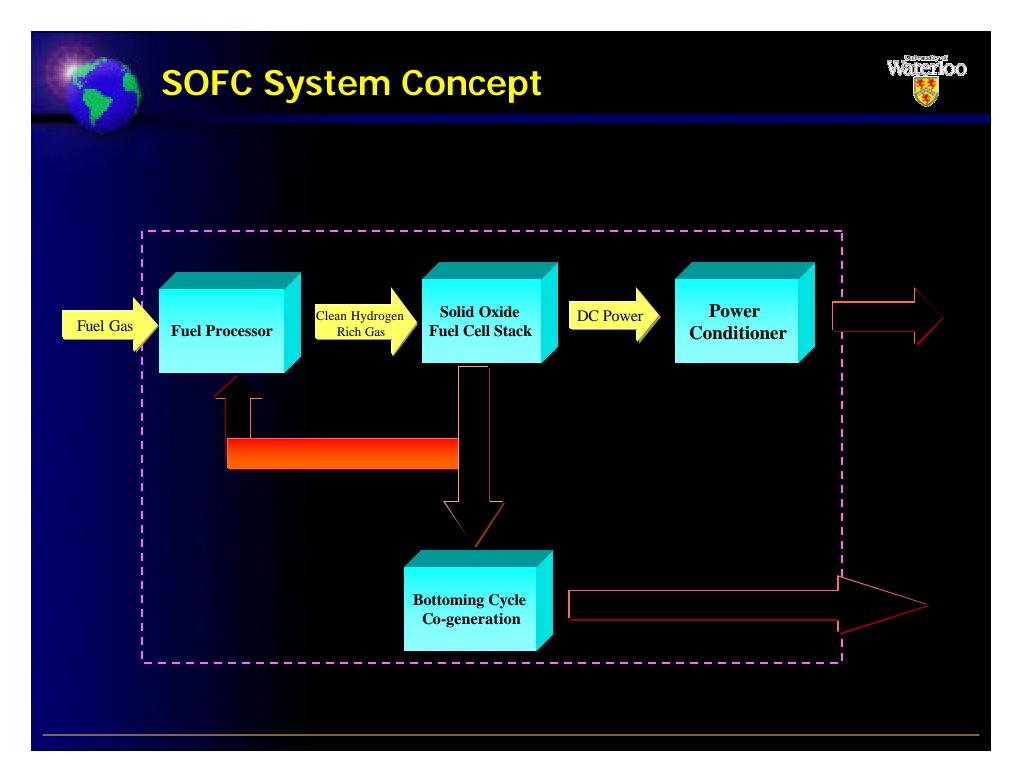
 examine potential SOFC-based power generation/CO<sub>2</sub> capture cycles at conceptual level

- SOFC cycle models in Aspen Plus:
  - develop SOFC (empirical) and process cycles models into Aspen Plus, allowing for integration, optimization and, eventually, costing

#### Mechanistic Model

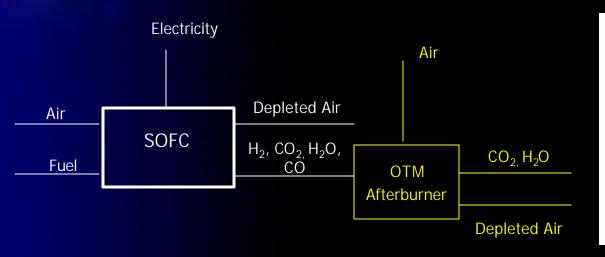
 develop a fundamental model to simulate fuel cell performance over a wide range of operating conditions, fuel compositions, and cell designs

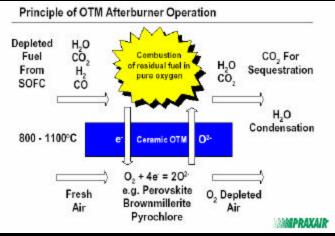


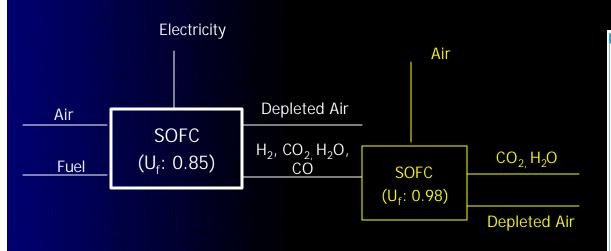


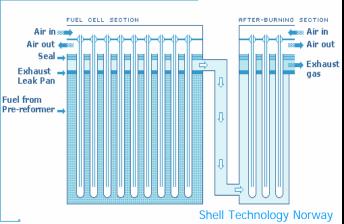
## **CO<sub>2</sub> Capture Using SOFC**





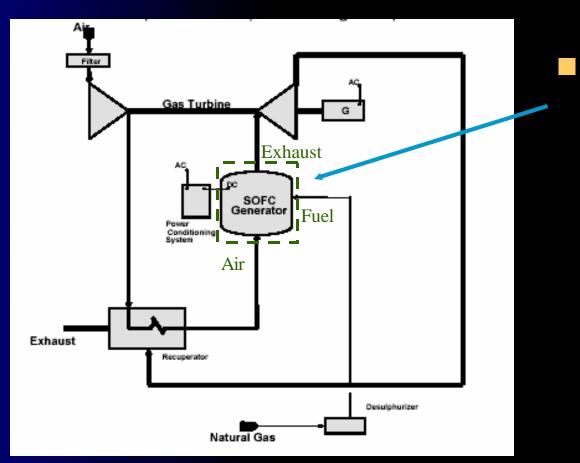






DNSEPTUAL DESIGN OF THE DEMONSTRATION UNIT

## **SOFC Modeling in Aspen Plus: Challenge**



How to develop a SOFC Model, which can

Waterloo

- Predict the fuel cell performance accurately
- Be implemented in Aspen Plus

## **SOFC Modeling in Aspen Plus: Approach**



#### Common Approach

Develop a complete
 SOFC stack model in a
 programming language
 such as Fortran or C++

 Link it to a commercial simulator (Aspen Plus, Hysis, Proll) as a userdefined model or subroutines.

#### Our Approach

 Incorporate a series of fuel cell performance curves (expressed by semiempirical equations) into Aspen Plus

 Develop the rest of SOFC using existing Aspen Plus unit operation models

#### **Aspen Plus SOFC Model** 30 9 15 Exhaust RECUPER Air HEATER2 14 Q4 CATHODE EJECTOR REFORMER HEATER1 AFTERBUR 13 12 1 Fuel ANODE Q1 SPLIT Q2 5 4 COOLER1 6

Based on the Siemens-Westinghouse natural gas feed tubular internal reforming SOFC technology

#### **Mechanistic Model - Objectives**



- Develop an accurate cell-level model to predict steady-state cell performance and flue gas compositions
- Investigate the influence of cell design, microstructure and operating variables on steady-state cell performance and its flue gas compositions
- Develop the cell performance map based on operation of H<sub>2</sub> and CO mixtures
- Generate parameters for correlations used in the AspenPlus model

### **Parameters To Be Investigated**

- Operating parameters
  - Inlet air and fuel temperature
  - Fuel and air utilization (U<sub>f</sub> & U<sub>a</sub>)
  - Inlet gas composition
  - Steam-to-carbon ratio
- Material parameters
  - Pore size
  - Porosity
  - Tortuosity factor
  - Composition of electronic/ionic conductors
- Design parameters
  - Cell geometry (length, width, etc.)
  - Electrode thickness
  - Electrolyte thickness

#### **Mechanistic Model - Methodology**



- Develop one- and two-dimensional mechanistic model of a single-cell SOFC considering H<sub>2</sub> and CO oxidations.
- Experimental setup and investigation
- Validation of the developed model
- Investigate the influence of cell design, microstructure and operating variables on steady-state cell performance and its flue gas compositions.
- Develop the cell performance map for mixtures of H<sub>2</sub> and CO

## **Experimental Setup and investigation**

Generate experimentally polarization curves for different situations

#### Example of proposed experimental plan

Fuel no.		Compo	osition	P(CO)	H <sub>2</sub> :CO	
	$H_2$	H <sub>2</sub> O	CO	$CO_2$	$\overline{P(CO) + P(H_2)}$	
	(%)	(%)	(%)	(%)		
<b>F</b> 1	80	20	0	0	0	1:0
F2	64.2	16.0	14.9	4.9	0.20	4:1
F3	38.8	9.7	38.8	12.6	0.50	1:1
F4	18.8	4.7	57.8	18.8	0.75	1:3
F5	0	0	75.5	24.5	1	0:1

#### **Preliminary Model Results- Model Validation**

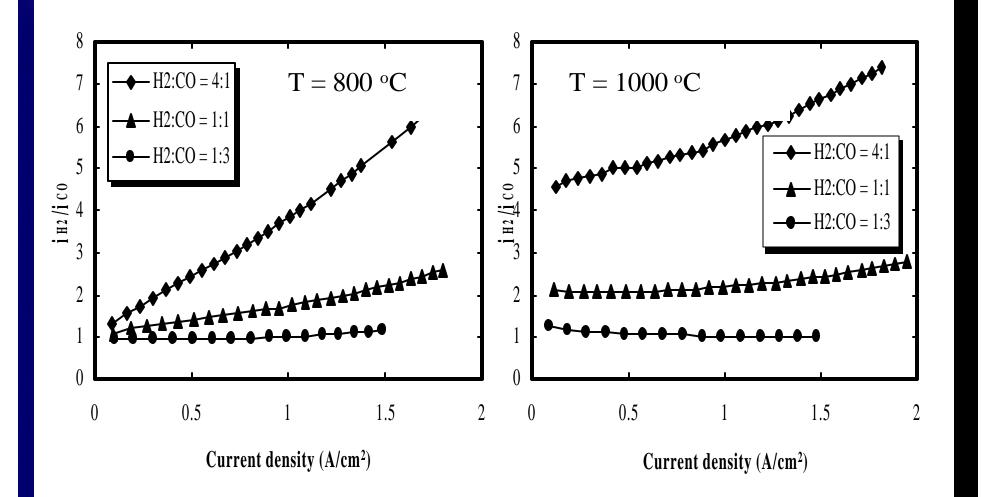


# Relative consumption of $H_2$ to CO (mol $H_2$ /mol CO) for the same concentration of $H_2$ and CO

Temp.	UW model	Yasuda <i>et al.</i> experiment (1999)
800 °C	1.1-2.6	1.9-2.3
1000 °C	2.0-2.6	2.3-3.1

Model agrees with published experimental data

#### Preliminary Model Results- Effect of gas compositions



#### Preliminary Model Results-Effect of Gas Compositions

- SOFC performance decreases as CO concentration increases
- H<sub>2</sub>:CO should be greater than 1:3 300 °C 09Cell voltage (V) 0.0 Cell voltage (V) 0.4 Cell voltage (V) 0.8 1000 °C Cell voltege ( 0.7 Increase CO 0.5 0.2 Increase CO  $\mathbf{0}$ 0.3 **Power density** (W/cm<sup>2</sup> 0.3 0.2 0.1  $W/cm^{-1}$ 1.2 **Power density** 0.8 H2:CO = 1:0H2:CO = 4:1ncrease CO - H2:CO = 1:0 + H2:CO = 4:1 -- H2:CO = 1:3 0.4 H2:CO = 1:1  $\rightarrow$  H2:CO = 0:1 0 -- H2:CO = 1:3 Ancrease CO  $\rightarrow$  H2:CO = 0:1 0.2 0.6 0.8 1.6 0 1.4 0.41.2 0 3 **Current density** (A/cm<sup>2</sup>) 0 2

Current density (A/cm<sup>2</sup>)

#### Achievements



#### Two technical papers (One accepted, One to be submitted)

 R. Suwanwarangkul, E. Croiset, M.W. Fowler, P.L. Douglas, E. Entchev and M. Douglas, "Performance Comparison of Fick's, the Dusty-gas and the Stefan-Maxwell Models to Predict the Concentration Overpotential in a SOFC Anode", J Power Sources, In press.

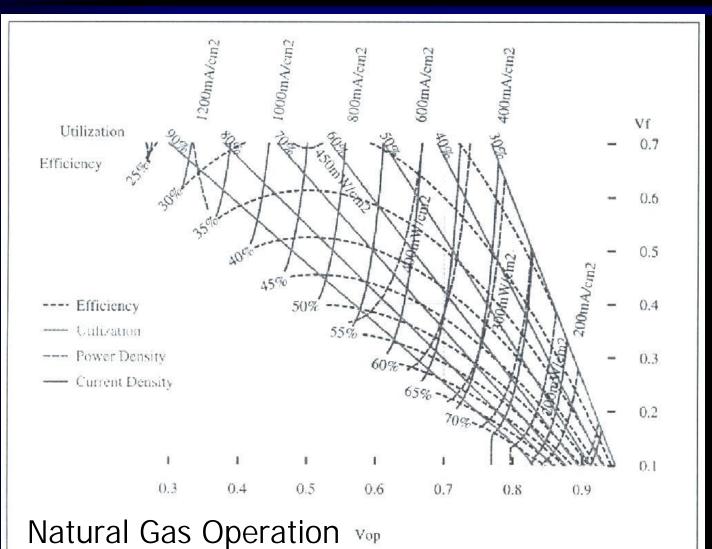
W. Zhang, E. Croiset, P.L. Douglas, M.W. Fowler, E. Entchev and M. Douglas, "Simulation of a Tubular Solid Oxide Fuel Cell Using AspenPlus Unit Operation Models", to be submitted by end of April.

#### One conference paper

 R. Suwanwarangkul, E. Croiset, M.W. Fowler, P.L. Douglas, E. Entchev and M. Douglas, "Modeling of Anode-supported SOFCs Operating with H<sub>2</sub> and CO Feed Mixtures", Proc. Of 8<sup>th</sup> International Symposium on Solid Oxide Fuel Cells (SOFC-VIII), S.C. Singhal, M. Dokiya (Eds.), 1348-1357 (2003).

## **Cell Performance Map**





SOFC Performance Map, H2O/CH4 = 2.0, 0.5 ohm-cm2

## **Design of Experiment**



Gas comp.	U <sub>f</sub>		U <sub>a</sub>		S/C ratio		T <sub>a</sub>		Τ <sub>f</sub>	
	High	Low	High	Low	High	Low	High	Low	High	Low
F1	V	V	V	V			V	V	V	V
F2	V	V			V	V				
F3	V	V			V	V				
F4	V	V			V	V				
F5	V	V	V	V			V	V	V	V

Each experiment must be performed 3 times.

- Interest experimental data:
  - Cell power
  - Exit gas compositions
  - Fuel and air flowrate
  - Exit fuel and air temperature